

06-720

Advanced Process Systems Engineering  
Homework 9

Spring, 2011  
Due: 4/18/11

1. Consider the reactor optimization problem given by:

$$\begin{aligned} \min \quad & L - 500 \int_0^L (T(t) - T_S) dt \\ \text{s.t.} \quad & \frac{dq}{dt} = 0.3(1 - q(t))\exp(20(1 - 1/T(t))), q(0) = 0 \\ & \frac{dT}{dt} = -1.5(T(t) - T_S) + 2/3 \frac{dq}{dt}, T(0) = 1 \end{aligned}$$

where  $q(t)$  and  $T(t)$  are the normalized reactor conversion and temperature, respectively, and the decision variables are  $T_S \in [0.5, 1]$  and  $L \in [0.5, 1.25]$ .

- (a) Derive the direct sensitivity equations for the DAEs in this problem.
  - (b) Using MATLAB or a similar package, apply the sequential approach to find the optimum values for the decision variables.
  - (c) How would you reformulate the problem so that the path constraint  $T(t) \leq 1.45$  can be enforced?
2. Consider the system of differential equations:

$$\begin{aligned} \frac{dz_1}{dt} &= z_2 \\ \frac{dz_2}{dt} &= 1600z_1 - (\pi^2 + 1600)\sin(\pi t) \end{aligned}$$

- (a) Show that the analytic solution of these differential equations are the same for the initial conditions  $z_1(0) = 0, z_2(0) = \pi$  and the boundary conditions  $z_1(0) = z_1(1) = 0$ .
- (b) Find the analytic solution for the initial and boundary value problems. Comment on the dichotomy of each system.

3. Consider the following reactor optimization problem.

$$\begin{aligned} \max \quad & c_2(1.0) \\ \text{s.t.} \quad & \frac{dc_1}{dt} = -k_1(T)c_1^2, c_1(0) = 1 \\ & \frac{dc_2}{dt} = k_1(T)c_1^2 - k_2(T)c_2, c_2(0) = 0 \end{aligned}$$

where  $k_1 = 4000 \exp(-2500/T)$ ,  $k_2 = 62000 \exp(-5000/T)$  and  $T \in [298, 398]$ . Discretize the temperature profile as piecewise constants over  $N_T$  periods and perform the following.

- (a) Derive the direct sensitivity equations for the DAEs in this problem.
- (b) Derive the adjoint sensitivity equations for the DAEs in this problem.
- (c) Solve using the sequential strategy with MATLAB or a similar package.
- (d) Solve using the multiple shooting strategy with MATLAB or a similar package.

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solution - HW 9

$$\text{Min } L = 500 \int_0^L (T - T_s) dt$$

$$\text{s.t. } \dot{q} = 0.3(1-q) \exp(20(1-\frac{1}{T}))$$

$$q(0) = 0$$

$$\dot{T} = -1.5(T(t) - T_s) + \frac{2}{3}\dot{q}$$

$$T(0) = 1$$

$$L \in [0.5, 1.25]; T_s \in [0.5, 1]$$

a) Sensitivity eqns.

- note that  $t \in [0, L]$  so we need to normalize lengths:  $t = \tau L$ ,  $\tau \in [0, 1]$   
 this leads to:

$$\text{Min } L = 500 q(1)$$

$$\frac{dq}{d\tau} = 0.3L(1-q) \exp(20(1-\frac{1}{T})),$$

$$q(0) = 0$$

$$\frac{dT}{d\tau} = -1.5L(T - T_s) +$$

$$+ 0.2L(1-q) \exp(20(1-\frac{1}{T}))$$

$$T(0) = 1$$

$$\frac{dz}{dt} = L(T - T_s), z(0) = 0$$

Sensitivity eqns (wrt  $T_s$  &  $L$ )

$$\dot{S}_{T_s} = (-0.3LS)_{T_s} \exp(20(1-\frac{1}{T}))$$

$$+ 0.3(1-q)L \exp(20(1-\frac{1}{T}))$$

$$+ \frac{6}{T^2}(1-q)L \exp(20(1-\frac{1}{T})) S_{T_s}$$

$$\dot{S}_{2T_3} = -0.3L S_{2T_3} \exp(20(1-\frac{1}{T})) + \frac{6(1-q)}{T^2} L \exp(20(1-\frac{1}{T})) S_{T_3}$$

$$S_{T_2} = -1.5(T-T_3) - 1.5L S_{T_2} + 0.2(1-q) \exp(20(1-\frac{1}{T})) + 0.2L \exp(20(1-\frac{1}{T})) \\ \left[ \frac{20(1-q)}{T^2} S_{T_2} = 0.2 S_{T_2} \right]$$

$$\dot{S}_{T_2} = -1.5L S_{T_3} + 1.5L + 0.2L \exp(20(1-\frac{1}{T})) \left[ \frac{20(1-q)}{T^2} S_{T_2} = 0.2 S_{T_2} \right]$$

$$S_{\delta^L} = (T-T_3) \quad S_{\delta^{T_3}} = -L \\ S_{ij}(0) = 0.$$

b) Solution of hot spot problem  
 (solved w/ AMPL as a test case with profiles below.)

c) In sequential approach, it is difficult to place bounds on states. One "trick" is to define

$\dot{z} = (\max(0, T-1.45))^2, z(0)=0$   
 and to impose  $z(t_f) \leq 2$  as a final time constraint. This violates L1C9 but is smaller.

Profiles for  $T(t) \leq 1.45$  are given on pg.

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# Dynamic Optimization of Hot Spot
Reactor - Problem 1 in HW 9

# This file implements the dynamic
optimization of a hot spot reactor.
# It uses the simultaneous approach
but is meant to provide a solution
# requested for the sequential
approach.

# Written by L. T. Biegler/ CMU, 4-
17-2011

param nfe;
let nfe:= 100;
set I:= 1..nfe;
set J:= 1..3;

param qinit :=0.;
param tinit :=1;
param zinit :=0;

param omega{J,J};

let omega[1,1] := 0.19681547722366;
let omega[1,2] :=0.39442431473909;
let omega[1,3] :=0.37640306270047;
let omega[2,1] := -0.06553542585020;
let omega[2,2] :=0.29207341166523;
let omega[2,3] :=0.51248582618842;
let omega[3,1] := 0.02377097434822;
let omega[3,2] :=-0.04154875212600;
let omega[3,3] :=0.1111111111111111;

param h{i in I} := 1/nfe;

# Initial guess of the decision
variables

var q{i in I,j in J} >= 0., <= 1., :=
0.5;
var t{i in I,j in J} >= 0., <=
10., := 10;
var z{i in I,j in J} >= 0., <=
10., := 1.;

var tt{i in I,j in J} >= 0., <=
10., := 1.;

var qdot{I,J};
var tdot{I,J};
var zdot{I,J};

var ts >= 0.05, <= 1.:= 0.7;
var ll >= 0.5, <= 1.25:= 0.8;
# var ll >= 0.5, <= 10.:= 0.8;
var q0{i in I} >=0, <=1, :=qinit;
var t0{i in I} >= 0, <= 10, := tinit;

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var tt0{i in I} >= 0, <= 10, := 1;
var z0{i in I} >= 0, <= 1, := zinit;
var qf >= 0, <= 1, := qinit;
var tf >= 0, <= 10, := tinit;
var zf >= 0, <= 10, := zinit;
var ttf >= 0, <= 10., := 1;

minimize phi: ll - 500*zf;

FECOLc{i in I, j in J}:
q[i,j]=(q0[i]+h[i]*sum{k in J}
(omega[k,j]*qdot[i,k])) ;

FECOLt{i in I, j in J}:
t[i,j]= (t0[i]+h[i]*sum{k in J}
(omega[k,j]*tdot[i,k])) ;

FECOLz{i in I, j in J}:
z[i,j]= (z0[i]+h[i]*sum{k in J}
(omega[k,j]*zdot[i,k])) ;

FECOLtt{i in I, j in J}:
tt[i,j]= tt0[i]+h[i]*sum{k in J}
(omega[k,j]*ll) ;

CONq{i in I diff {1}}:
q0[i] = (q0[i-1] + h[i-1]*sum{j in J}
(qdot[i-1,j]*omega[j,3]));

CONt{i in I diff {1}}:
t0[i] = (t0[i-1] + h[i-1]*sum{j in J}
(tdot[i-1,j]*omega[j,3]));

CONz{i in I diff {1}}:
z0[i] = (z0[i-1] + h[i-1]*sum{j in J}
(zdot[i-1,j]*omega[j,3]));

CONtt{i in I diff {1}}:
tt0[i] = tt0[i-1] + h[i-1]*sum{j in J}
(ll*omega[j,3]);

ODEq{i in I, j in J}:
qdot[i,j] = ll*(0.3*(1-
q[i,j])*exp(20*(1-1/t[i,j])));

ODEt{i in I, j in J}:
tdot[i,j] = ll*(-1.5*(t[i,j]-ts) +
2/3*qdot[i,j]);

ODEz{i in I, j in J}:
zdot[i,j] = ll*(t[i,j]-ts);

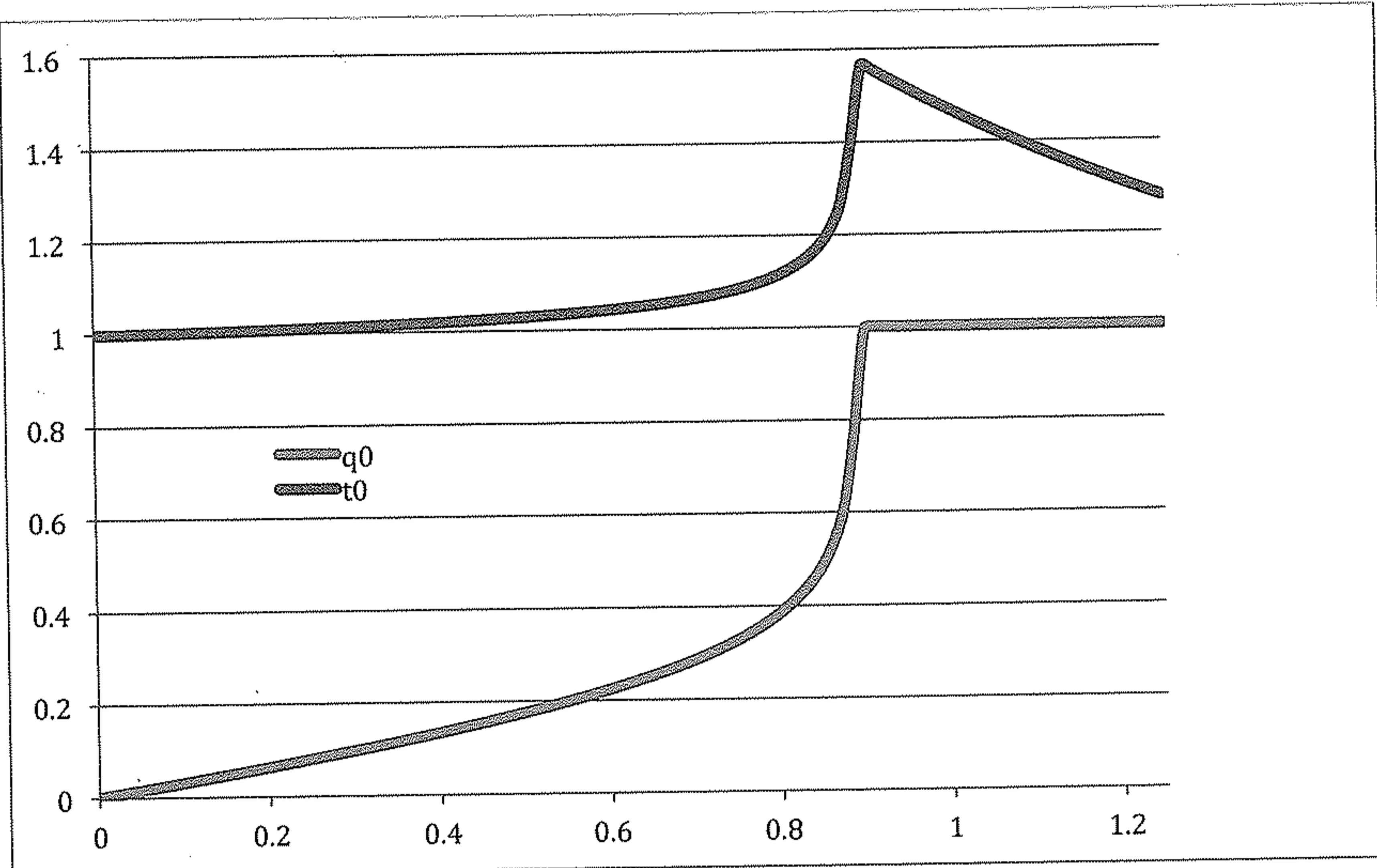
FINq: qf = q[nfe, 3];
FINt: tf = t[nfe, 3];
FINz: zf = z[nfe, 3];

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FINtt: ttf = tt[nfe, 3];           ITT: tt0[1] = 0;
IQ: q0[1] = qinit;                 option solver Ipopt;
IT: t0[1] = tinit;                  solve;
IZ: z0[1] = zinit;

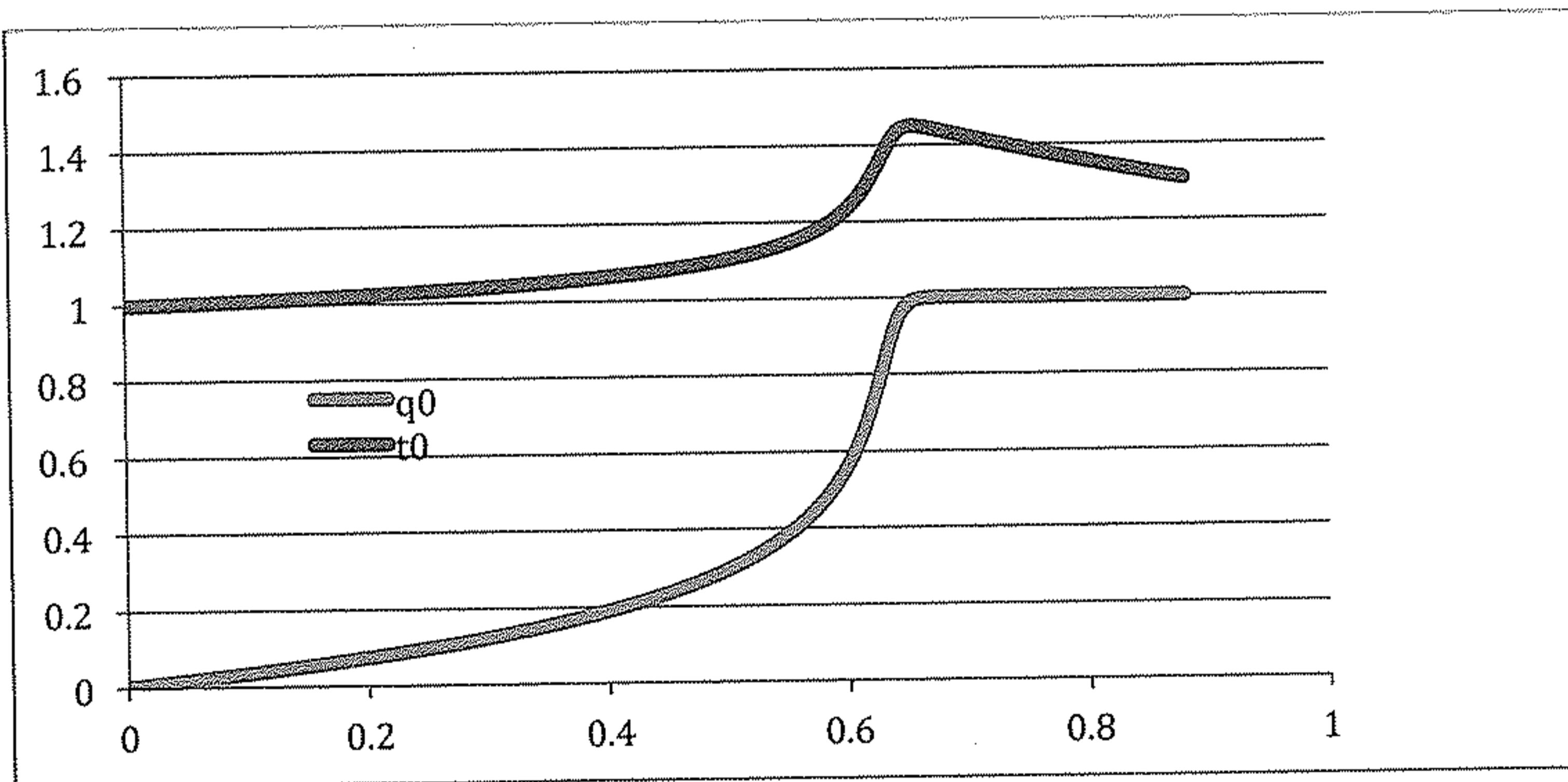
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```

add constraint
tc{i in I, j in J}: t[i,j] <= 1.45;
solve;

```



2.

Boile problem

$$\begin{aligned} \dot{z}_1 &= z_2 \\ \dot{z}_2 &= 1600 z_1 - (\pi^2 + 1600) \sin \pi t \end{aligned}$$

a)

$$z_1(0) = 0$$

has solution

$$z_1(0) = \pi$$

$$z_1 = \sin \pi t$$

$$z_2 = \pi \cos \pi t$$

This is same solution as!

$$z_1(0) = 0$$

$$z_1(1) = 0$$

b)

For initial value problem, the unstable mode is not "pinned down" and there is no dichotomy.

For boundary value problem, both stable & unstable modes are "pinned down".

$$3. \quad \min - c_2(1.0)$$

s.t.

$$\dot{c}_1 = -k_1(T) c_1^2, \quad c_1(0) = 1$$

$$\dot{c}_2 = k_1(T) c_1^2 - k_2(T) c_2$$

$$c_2(0) = 0$$

$$k_1 = 4000 \exp(-2500/T)$$

$$k_2 = 62000 \exp(-5000/T)$$

$$T \in [298, 3498]$$

a) Sensitivity eqns. wrt  $T_j$

$$(1) \quad \dot{S}_{1j} = -2k_1(T_j) c_1 S_{1j}, \quad S_{1j}(0) = 0$$

$$(2) \quad \dot{S}_{2j} = 2k_1(T_j) c_1 S_{1j} - k_2(T_j) S_{2j}, \quad S_{2j}(0) = 0$$

for  $t \notin \{t_{bj+}, t_j\}$

$$(3) \quad \dot{S}_{1j} = -2k_1(T_j) c_1 S_{1j} - \frac{\partial k_1}{\partial T_j} c_1^2, \quad S_{1j}(0) = 0$$

$$(4) \quad \dot{S}_{2j} = 2k_1(T_j) c_1 S_{1j} - k_2(T_j) S_{2j}, \quad S_{2j}(0) = 0$$

$+ \frac{\partial k_1}{\partial T_j} c_1^2 - \frac{\partial k_2}{\partial T_j} c_2$

$$\frac{\partial k_1}{\partial T_j} = \frac{1.6}{T^2} \exp(-2500/T)$$

$$\frac{\partial k_2}{\partial T_j} = \frac{12.4}{T^2} \exp(-5000/T)$$

$$\frac{dS_{2j}}{dT_j} = -S_{2j}(1)$$

(5)

b) Adjoint sensitivity

$$\lambda^T f = \lambda_1 (-k_1(T)c_1^2) + \lambda_2 (k_1(T)c_1^2 - k_2(T)c_2)$$

$$\lambda_1 = -2k_1(T)c_1(\lambda_1, -\lambda_2), \quad \lambda_1(1) = 0$$

$$\lambda_2 = \lambda_2 k_2(T), \quad \lambda_2(1) = -1$$

$$\frac{dc}{dT_j} = \int_{t_{j-1}}^{t_j} \left( (\lambda_2 - \lambda_1) \frac{\partial k_1}{\partial T_j} c_1^2 - \lambda_2 \frac{\partial k_2}{\partial T_j} c_2 \right) dt$$

c) Solution w/ sequential approach.

$$\text{solve } \min -c_2(1)$$

$$\text{s.t. } 298 \leq T_j \leq 398$$

with  $c_1(t), c_2(t)$  and  $\frac{\partial c_2}{\partial T_j}$   
evaluated from parts a) or b).

The solution is on next page.

d) Solution with multiple shooting

$$\text{solve } \min_{\tilde{c}_1, \tilde{c}_2} -c_2(N)$$

$$\text{s.t. } 298 \leq T_j \leq 398$$

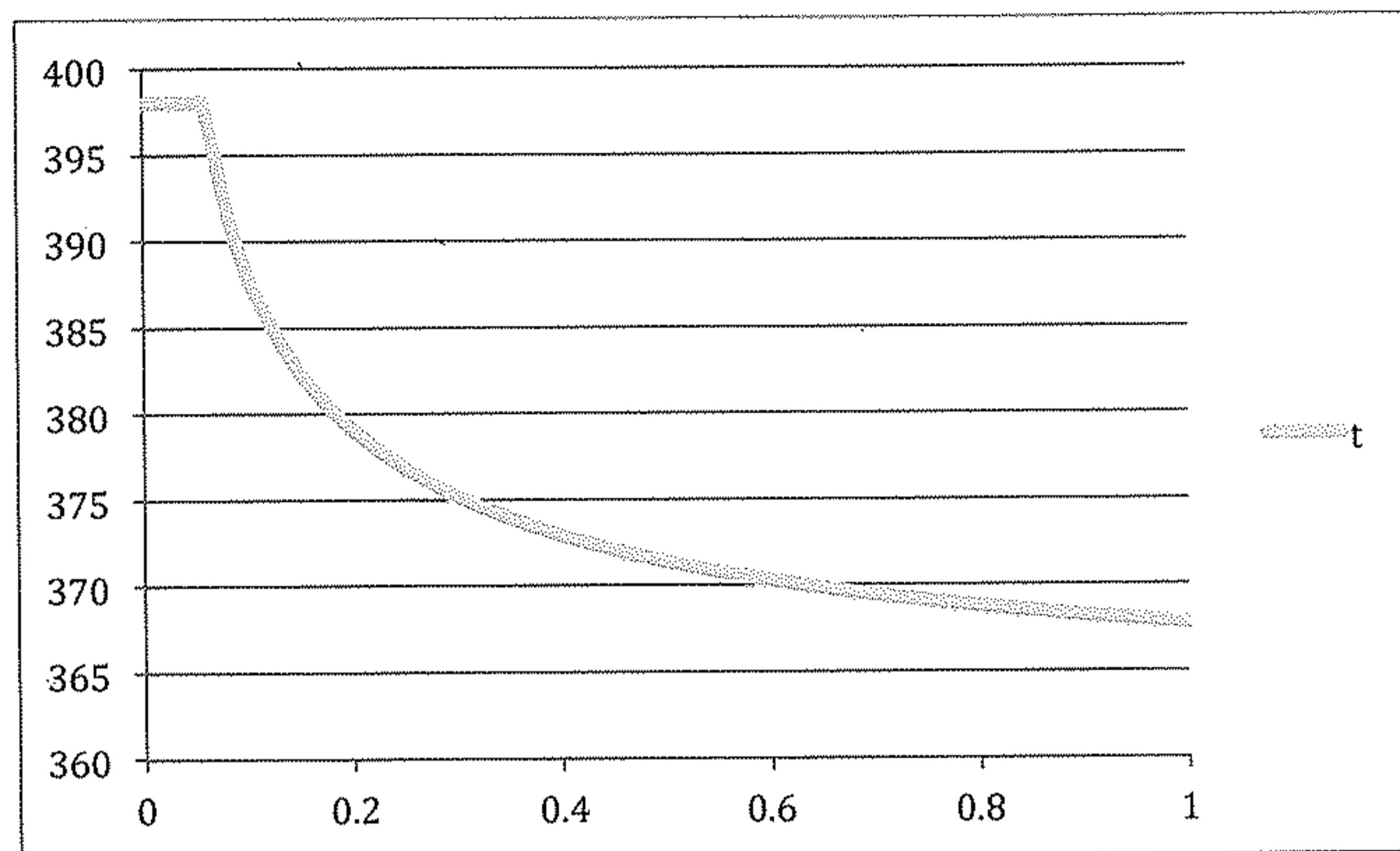
$$c_{1,j}(t_j) - \bar{c}_{1,j} = 0$$

$$c_{2,j}(t_j) - \bar{c}_{2,j} = 0$$

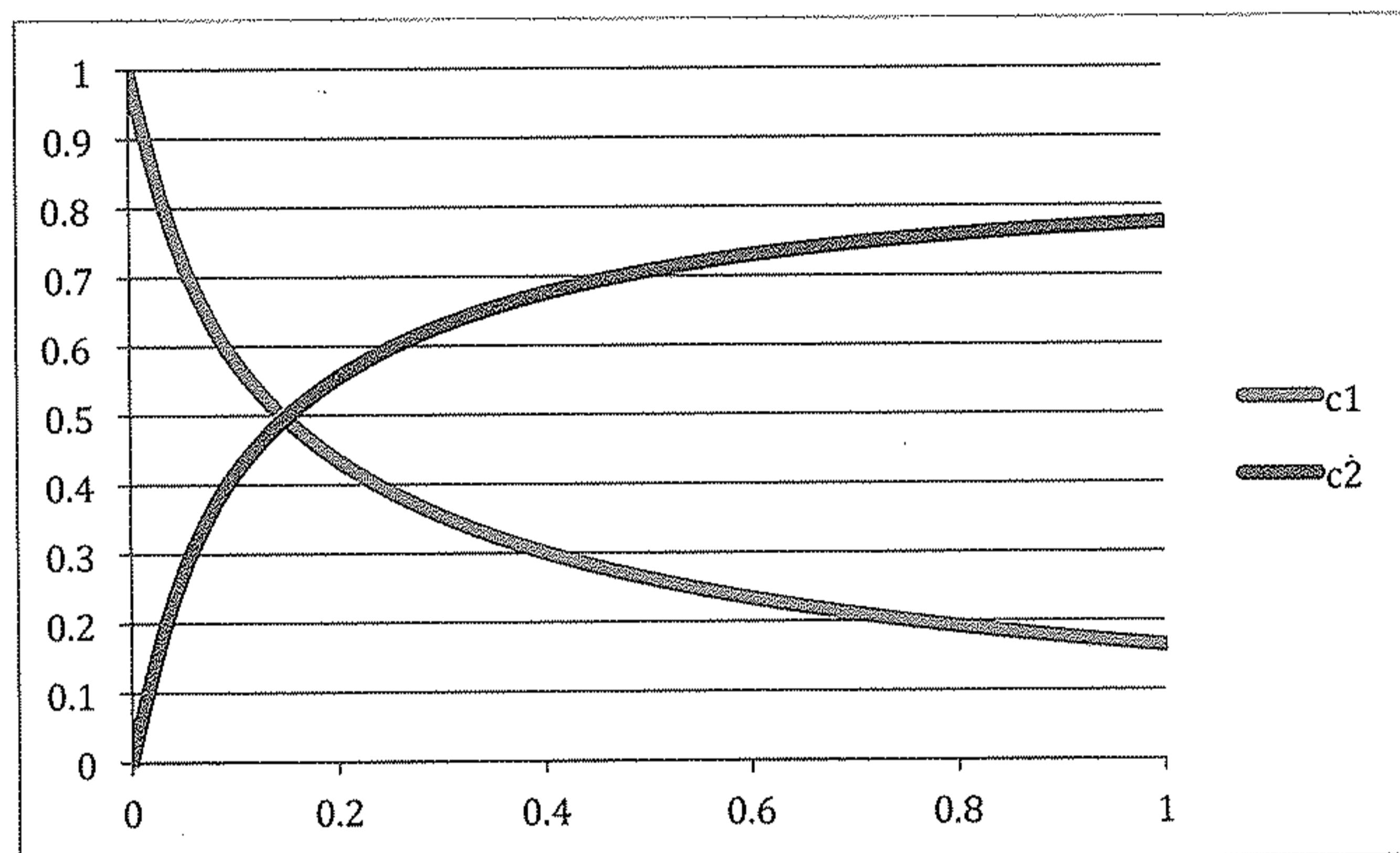
$j=1, \dots, N-1$

where  $\bar{c}_{1,j}, \bar{c}_{2,j}$  are also initial  
conditions for each segment of

### Solution Profiles Nonisothermal Batch Reactor (Max c2(1))



Optimal Temperature Profile



Optimal Concentration Profiles

```
# Dynamic Optimization of Hot  
Spot Reactor - Problem 1 in HW  
9
```

```
# This file implements the  
dynamic optimization of a  
nonisothermal
```

```
# batch reactor. It uses the  
simultaneous approach but is  
meant to  
# provide a solution requested  
for the sequential or multiple  
shooting  
# approach.
```

```

# Written by L. T. Biegler/
CMU, 4-17-2011

param nfe;
let nfe:= 20;
set I:= 1..nfe;
set J:= 1..3;

param clinit :=1.0;
param c2init :=0.0;

param omega{J,J};

let omega[1,1] :=
0.19681547722366;
let
omega[1,2] :=0.39442431473909;
let
omega[1,3] :=0.37640306270047;
let omega[2,1] := -
0.06553542585020;
let
omega[2,2] :=0.29207341166523;
let
omega[2,3] :=0.51248582618842;
let omega[3,1] :=
0.02377097434822;
let omega[3,2] :=-
0.04154875212600;
let
omega[3,3] :=0.1111111111111111;

param h{i in I} := 1/nfe;

# Initial guess of the decision
variables

var c1{i in I,j in J} >= 0., <=
1., := 0.5;
var c2{i in I,j in J} >= 0., <=
1., := 0.5;
var t{i in I,j in J} >= 298.,
<= 398., := 350;
var tt{i in I,j in J} >= 0.;
var c1dot{I,J};
var c2dot{I,J};

var c10{i in I} >=0, <=1, :=
0.5;
var c20{i in I} >=0, <=1, :=
0.5;
var tt0{i in I} >= 0;
var c1f >= 0, <= 1, := 0.5;
var c2f >= 0, <= 1, := 0.5;
var ttf >= 0;

minimize phi: -c2f;

FECOLc1{i in I, j in J}:
c1[i,j]=(c10[i]+h[i]*sum{k in
J}
(omega[k,j]*c1dot[i,k])) ;

FECOLc2{i in I, j in J}:
c2[i,j]=(c20[i]+h[i]*sum{k in
J}
(omega[k,j]*c2dot[i,k])) ;

FECOLtt{i in I, j in J}:
tt[i,j]= tt0[i]+h[i]*sum{k in
J} (omega[k,j]) ;

CONc1{i in I diff {1}}:
c10[i] = (c10[i-1] + h[i-
1]*sum{j in J} (c1dot[i-
1,j]*omega[j,3]));

CONc2{i in I diff {1}}:
c20[i] = (c20[i-1] + h[i-
1]*sum{j in J} (c2dot[i-
1,j]*omega[j,3]));

CONtt{i in I diff {1}}:
tt0[i] = tt0[i-1] + h[i-
1]*sum{j in J} (omega[j,3]);

ODE1{i in I, j in J}:
c1dot[i,j] = -4000*exp(-
2500/t[i,j])*c1[i,j]*c1[i,j];

ODE2{i in I, j in J}:
c2dot[i,j] = 4000*exp(-
2500/t[i,j])*c1[i,j]*c1[i,j]
- 62000*exp(-
5000/t[i,j])*c2[i,j];

FINc1: c1f = c1[nfe, 3];
FINc2: c2f = c2[nfe, 3];
FINtt: ttf = tt[nfe, 3];

IC1: c10[1] = clinit;
IC2: c20[1] = c2init;
ITT: tt0[1] = 0;

option solver Ipopt;

solve;

```

The state equations:

$$\dot{c}_{1j} = -k_1(T_j) c_{1j}^2, \quad c_{1j}(t_{j+}) = \bar{c}_{1j}$$

$$\dot{c}_{2j} = k_1(T_j) c_{1j}^2 - k_2(T_j) c_{2j}, \quad c_{2j}(t_{j+}) = \bar{c}_{2j}$$

Respective eqns for each component are:  
 the same as (3)-(4) for  $T_j$ , but  
 not (1)-(2). The initial conditions  
 concentrations are given by:

$$\dot{\bar{s}}_{1j} = 2k_1(T_j) \bar{s}_{1j}, \quad \bar{s}_{1j}(t_{j+}) = 1$$

$$\dot{\bar{s}}_{2j} = 2k_1(T_j) \bar{s}_{1j} \bar{s}_{2j} - k_2(T_j) \bar{s}_{2j}, \quad \bar{s}_{2j}(t_{j+}) = 1$$

for  $t \in [t_{j+}, t_f]$ ,  $j=2, \dots, NT$

The solution profiles are on the  
 next page.